

Research on the Carbon Dioxide Emission Factor as a Result of Fuel Combustion

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The present paper first discusses a calculation model for the complete combustion of fuels – with the minimum amount of air needed – whose volumetric and mass composition is known. It then describes evaluation models for the heat resulting from fuel combustion, i.e., superior and inferior caloric power value. In this context, the carbon dioxide emission factors for fuel and biofuel combustion, respectively, are evaluated. The results obtained have allowed a comparative analysis regarding carbon dioxide emission.

Keywords: complete fuel combustion, biofuels, carbon dioxide emission factor

The meteorological phenomena we have been facing lately are the direct or indirect result of human activity. They are the consequences of climate change. Ensuring energy security with competitive and *clean* energy, taking into account the limitation of climate change, represents a major challenge for the European Union.

The vision of the current European energy policy is in line with the concept of sustainable development and it refers, among others, to the reduction of greenhouse gas (GHG) emissions [1]. Nationally, policies and action plans to reduce GHG emissions are a key element in limiting the effects of climate change on the environment, the economy and society. They are in line with the European requirements regarding this domain. In this respect, the National Strategy on Climate Change of Romania 2013-2020, adopted in July 2013, and the National Strategy on Climate Change and Economic Growth regarding low carbon emissions have been published, identifying the main sectors for priority actions for reducing GHG emissions, such as energy, transport, industrial processes, agriculture and rural development, urban development, waste management, water and forestry [2].

In 2016, compared to 2015, Romania recorded a 1.4% drop in CO₂ emissions from fossil fuel combustion. Carbon dioxide emissions in the EU dropped by 0.4% overall. In 2016, the share of CO₂ emissions in Romania accounted for 2.1% of total EU CO₂ emissions [3].

Periodic statistical surveys on the production of electricity and heat, resources and electric power consumption, heat, fuels, fuels and lubricants, the monitoring of carbon dioxide emissions, have led to their classification according to various criteria [4-8].

Reducing greenhouse gas emissions and, consequently, preventing dangerous climate change can be achieved by reducing energy consumption and by using secondary energy sources and renewable energy sources, respectively [9].

Fuels are substances that burn, producing heat, and contain the following combustible elements: carbon, hydrogen and sulfur. A fuel must meet certain conditions, namely: to be easily obtained from nature, not to be toxic, to be inexpensive and in sufficient quantity, so that the cost of the heat obtained be competitive on the energy market. It is worth mentioning that the fuels analysed are stored ones.

The classification of fuels is done according to certain criteria, including:

- state of aggregation - solid (coal, wood), liquid (petroleum products) and gaseous (natural gas, well gas);
- origin - natural (wood, coal, oil, natural gas, well gas); artificial, derived from industrial processes (diesel, petrol, hydrogen, liquefied petroleum gas, biofuels) [10].

An alternative to fossil fuels is biofuels. They can be used as pure or mixed fuel with a fossil fuel. Bioethanol is mainly obtained from cereals or cane and is equivalent to petrol. Biodiesel (ethyl stearate and methyl linoleate) is mainly derived from oilseeds such as rapeseed, corn, soybeans and is similar to diesel oil.

As regards solid and liquid fuels, as well as gaseous fuels, the mass and volumetric composition, respectively - the latter only in the case of gaseous ones - are expressed by specific relations [10].

For liquid petroleum fuels whose relative density, ρ_{15}^{15} , is known, the carbon and the hydrogen fractions can be calculated using semi-empirical relations [10, 11].

If a chemical formula is known for a fuel, then the mass fractions can be calculated using relations [10]:

$$g_C = \frac{12m}{12m + n + 16r}; \quad g_H = \frac{n}{12m + n + 16r};$$
$$g_O = \frac{16r}{12m + n + 16r} \quad (1)$$

For a fuel whose mass composition is known, the mass of carbon dioxide at full combustion is calculated as follows:

$$m_{CO_2} = \frac{g_C}{12} M_{CO_2} \quad (2)$$

In relation (2), the carbon dioxide mass has the unit of measurement kg CO₂/kg of fuel. For gaseous hydrocarbons whose volumetric composition is given, the volume of carbon dioxide, expressed in m³ CO₂/m³ of fuel resulting from full combustion, is obtained by summing up the volumes of carbon dioxide resulting from the combustion of hydrocarbons and carbon monoxide, to which the carbon dioxide that may exist in the fuel's original composition is added:

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$$V_{CO_2} = \sum (m r_{CmHn})_i + r_{CO} + r_{CO_2} \quad (3)$$

In this case, the mass of carbon dioxide, with the unit of measurement of CO_2/m^3_N of fuel, is obtained as follows:

$$m_{CO_2} = \frac{M_{CO_2}}{22,414} \cdot V_{CO_2} \quad (4)$$

Fuels are characterized by the heat produced by the complete combustion of the fuel quantity unit, i.e., the calorific value, with the minimum amount of air needed. There are two types of calorific value:

- superior calorific value H_s - when the vapours contained in the combustion gases are discharged in liquid state - in other words, latent condensation heat is released into the combustion space;

- inferior calorific value H_i - in which case the combustion gases are discharged with gaseous water vapours.

Although it is obvious that the gross calorific value is higher than the net one, often for technical reasons (water in liquid state can be combined with some combustion gas components, forming corrosive fluids), it is recommended that combustion gases be discharged while the water they contain is in vapour state. As a result, practically, it is net calorific value that is of interest most of the times [6].

If a fuel does not contain water, the mathematical relationship between the inferior and the superior calorific value is as follows:

$$H_i = H_s - 2510 \cdot 9 g_H \quad (5)$$

The calorific value of a biofuel, whose chemical formula is $C_m H_n O_r$, and which does not contain water, is calculated as follows:

$$H_i = 33\,900 g_C + 120\,120 \left(g_H - \frac{g_O}{8} \right) \quad (6)$$

By applying relationships (5) and (6) results expressed in kJ/kg are obtained; g_i are decimals.

For mixtures of gaseous fuels, the calorific value is calculated as follows [10, 11]:

$$H_{am} = \sum_{i=1}^n r_i H_i \quad (7)$$

In the case of liquid petroleum fuels, semi-empirical relations [10, 11] can be used to calculate the calorific value.

The release of carbon dioxide takes place both during the combustion of fossil fuels and biofuels. In order to compare the polluting effects of fuel combustion, the carbon dioxide emission factor is used, being defined by the relation below:

$$\varepsilon_{CO_2} = \frac{m_{CO_2}}{H} \quad (8)$$

Depending on the carbon dioxide mass/inferior calorific value ratio, on the one hand, and the carbon dioxide mass/superior calorific value ratio, on the other hand, the following can be distinguished:

- $\varepsilon_{CO_2,I}$ carbon dioxide emission relative to the inferior calorific value;

- $\varepsilon_{CO_2,S}$ carbon dioxide emission relative to the superior calorific value for fuels whose moisture content is zero percent [6].

By using relations (1), (2), (5), (6) and (8) the following relations are suggested for the calculation of the carbon dioxide emission factor [5]:

- $\varepsilon_{CO_2,I}$ carbon dioxide emission relative to the inferior calorific value [g CO_2 /kWh]:

$$\varepsilon_{CO_2,I} = \frac{1000 m}{2.568 m + 0.758 n - 1.517 r} \quad (9)$$

- $\varepsilon_{CO_2,S}$ carbon dioxide emission relative to the superior calorific value [g CO_2 /kWh]:

$$\varepsilon_{CO_2,S} = \frac{1000 m}{2.568 m + 0.901 n - 1.517 r} \quad (10)$$

In the relationships above m, n, r are the coefficients of the chemical formula $C_m H_n O_r$.

For the calculation of the carbon dioxide emission factor, in the case of liquid petroleum fuel burning, appropriate relations have been proposed for liquid petroleum fuels that contain hydrogen and carbon only [6].

Experimental part

A large number of fuel samples in all aggregation states - gaseous, liquid and solid - were analysed.

After the chromatographic analysis reports of certain gas mixtures were analysed, five samples were considered to be representative (table 1). The composition of the gaseous samples was analysed in specialized and authorised laboratories (table 2).

According to the reports containing the results of the chromatographic analyses for gases GL1, GA1, GA2, GT1, the analyses were conducted using the VARIAN CP-3800 (fig. 1).



Fig. 1. Varian CP -3800 Gas Chromatograph

Name of gas mixture	Symbol	Sample characterisation	Origin of analysis report
Free gas	GL1	Mixture of natural gas extracted from a well (free gas)	Analysis performed in authorised laboratory
Associated gas 1	GA1	Oil well gas mixture (associated gas)	Analysis performed in authorised laboratory
Associated gas 2	GA2	Oil well gas mixture (associated gas)	Analysis performed in authorised laboratory
Gases in the transportation pipeline	GT1	Gas mixture taken from the transportation pipeline	Analysis performed in authorised laboratory
Shale gas	Gsist	Burning, shale gas mixture	Composition taken from the literature [12]

Table 1
NAME OF GASEOUS MIXTURES

Composition	GL1	GA1	GA2	GT1	Gsist
	Volumetric fraction, %				
Oxygen - O ₂	0	0	0	0	2
Carbon Monoxide - CO	0	0	0	0	0
Azote - N ₂	0.154	1.238	0.584	0.1242	0
Carbon dioxide - CO ₂	0.2522	0.669	1.068	0.3307	0
Methane - CH ₄	95.9568	92.018	93.776	98.3678	80
Ethan - C ₂ H ₆	1.9231	3.105	2.544	0.7625	12
Prophan - C ₃ H ₈	0.78	1.662	1.083	0.231	6
iso-Butane - C ₄ H ₁₀	0.1959	0.294	0.265	0.0461	0
n-Butane - C ₄ H ₁₀	0.2682	0.453	0.257	0.0588	0
iso-Pentane - C ₅ H ₁₂	0.1324	0.172	0.102	0.0161	0
n-Pentane - C ₅ H ₁₂	0.0882	0.152	0.059	0.0097	0
Hexane - C ₆ H ₁₄	0.1115	0.126	0.081	0.0244	0
Heptane - C ₇ H ₁₆	0.0935	0.092	0.05	0.0182	0
Octane - C ₈ H ₁₈	0.0387	0.017	0.052	0.0079	0
Nonane - C ₉ H ₂₀	0.0055	0.001	0.03	0.0026	0
Hydrogen sulfide - H ₂ S	0	0.001	0.049	0	0
Total	100	100	100	100	100

Table 2
RESULTS OF THE
CHROMATOGRAPHIC
ANALYSIS OF GASEOUS
MIXTURES

Liquid fuels	Relative density (the density of the liquid fuels relative to the water, at 15 °C) ρ_{15}^{15}
Gasoline	0.7498
Disel fuel	0.8398
Liquefied petroleum gases	0.5346

Table 3
CHARACTERISTICS OF LIQUID FUELS

Solid fuels	Composition, %					
	g_C	g_H	g_O	g_N	g_S	
Anthracite	95.87	1.13	1.879	0.251	-	
Pit coal	84.23	4.61	9.5	-	1.66	
Lignite (Filipești de Pădure)	64.9	5.52	25.79	1	2.79	
Wood	Hardwood	50.5	6.10	42.8	0.6	-
	Softwood	51	6.15	42.25	0.6	-

Table 4
CHEMICAL COMPOSITION OF SOLID FUELS

Solid Fuels	Superior caloric power, kJ/kg	Inferior caloric power, kJ/kg	
Anthracite	24069	23593	
Pit coal	16894	16371	
Lignite	7552	6136	
Wood	Hardwood	20026	9258
	Softwood	20456	9500

Table 5
CALORIFIC VALUES OF SOLID FUELS

The CP-3800 GC is a gas chromatograph with a flexible platform for single, dual or three- channel configuration. The CP-3800 Gas Chromatograph allows upgrades to a multi-valve, multi-column configuration to handle complex analyses.

It is worth mentioning that after the research was conducted data regarding shale gas were collected from the literature. In Romania there is no shale gas exploitation.

The characteristics of the liquid petroleum fuels (considered representative) necessary for the calculation of the carbon dioxide emission factor are presented in table 3. They were taken from delivery certificates provided by companies that are engaged in the production or distribution of liquid petroleum products.

Table 4 contains the chemical composition of the selected solid fuels, whereas table 5 contains the gross and net calorific values, according to the literature [13].

The research carried out also included biofuels. Their names and chemical formulae are displayed in table 6.

Results and discussions

In order to assess the carbon dioxide emission resulting from the combustion of the analysed fuels relationships (8), (9) and (10) were used.

As regards gaseous fuels, the results obtained from the calculation of the carbon dioxide mass are shown in table 7.

The net and gross calorific values for samples GL1, GA1, GA2 and GT1 are taken from the chromatographic analysis reports. For shale gas these values are obtained by calculation [7], relation (7).

Table 7 shows that the calorific value of shale gas is higher than the one of the other gas mixtures.

Biofuel	Chemical formula	Sample characterisation
Ethanol	C ₂ H ₆ O	Ethanol can replace petrol or can be blended with it in certain proportions;
Ethyl stearate	C ₂₀ H ₄₀ O ₂	Ethyl stearate may replace – wholly or partly – diesel fuel.
Methyl linoleate	C ₁₉ H ₃₄ O ₂	Methyl linoleate may replace – wholly or partly – diesel fuel.

Table 6
NAMES OF BIOFUELS

Table 7
RESULTS OF CARBON DIOXIDE MASS AND CALORIFIC VALUE CALCULATION FOR GASEOUS MIXTURES

Compound	GLI	GAI	GA2	GTI	Gsist
Carbon dioxide mass m_{CO_2} , [kg CO ₂ /m ³ _N comb]	2.0813	2.1458	2.0918	1.9946	2.3949
Inferior caloric power, H_i [kJ / m ³ _N comb]	35800	36400	35700	34400	41974.1
Inferior caloric power, H_i [kWh / m ³ _N comb]	9.972	10.137	9.941	9.5567	11.659
Superior caloric power, H_s [kJ / m ³ _N comb]	39700	40400	39600	38100	46444.02
Superior caloric power, H_s [kWh / m ³ _N comb]	11.064	11.226	11.016	10.608	12.901

Table 8 contains the results obtained from the calculations for liquid fuels.

According to table 8, the calorific value of LPG is highest compared to the other liquid fuels analyzed.

As regards solid fuels, the calculation results are shown in table 9.

The results obtained from the calculation for biofuels are displayed in table 10.

Table 11 contains the carbon emission factor of the analysed fuels.

As shown in table 11, there is a decreasing distribution of fuel relative to the value of the carbon dioxide emission factor:

$$\mathcal{E}_{CO_2, S, Solid\ fuel} > \mathcal{E}_{CO_2, S, Liquid\ fuel} > \mathcal{E}_{CO_2, S, Gaseous\ fuel}$$

One of the conclusions to be highlighted in table 11 is that the values of the carbon dioxide emission factor corresponding to shale gas burning are the lowest.

Liquid fuels	Gasolina	Disel fuel	Liquefied petroleum gases
Carbon mass fraction, g_c	0.8525	0.8659	0.8202
Hydrogen mass fraction, g_H	0.1475	0.1341	0.1798
Carbon dioxide mass m_{CO_2} , [kg CO ₂ /kg]	3.126	3.175	3.007
Inferior caloric power, H_i [kJ / kg]	43866.69	42893.94	45615.13
Superior caloric power, H_s [kJ / kg]	47198.72	45921.68	49677.04

Table 8
RESULTS OF THE CALCULATION OF LIQUID FUEL MASS FRACTION, CARBON DIOXIDE MASS AND CALORIFIC VALUE

Solid fuels	Anthracite	Pit coal	Lignite	Wood	
				Hardwood	Softwood
Carbon mass fraction, g_c	0.9587	0.8423	0.6490	0.5050	0.5100
Hydrogen mass fraction, g_H	0.0413	0.1577	0.3510	0.4950	0.4900
Carbon dioxide mass, m_{CO_2} , [kg CO ₂ /m ³ _N comb]	3.515	3.088	2.379	1.8520	1.8700

Table 9
RESULTS OF THE CALCULATION OF SOLID FUEL MASS FRACTION AND CARBON DIOXIDE MASS

Biofuels	Ethanol	Ethyl stearate	Methyl linoleate
Carbon mass fraction, g_c	0.5217	0.7692	0.7756
Hydrogen mass fraction, g_H	0.1304	0.1282	0.1156
Oxygen mass fraction, g_o	0.3479	0.1026	0.1088
Inferior caloric power, H_i [kJ / m ³ _N]	28125.56	39934.73	38545.1
Superior caloric power, H_s [kJ / m ³ _N]	31071.29	42830.77	41156.50
Carbon dioxide mass, m_{CO_2} , [kg CO ₂ /m ³ _N comb]	1.913	2.82	2.844

Table 10
CALCULATION RESULTS FOR BIOFUELS

Fuels		Carbon dioxide emission relative to the inferior caloric power [g CO ₂ /kWh]	Carbon dioxide emission relative to the superior caloric power [g CO ₂ /kWh]
Lignite		1396	1134
Wood	Hardwood	720	330
	Softwood	709	330
Pit coal		679	658
Anthracite		536	526
Methyl linoleate		266	249
Diesel fuel		266	248
Gasoline		257	238
Ethyl stearate		254	237
Ethanol		245	222
Liquefied petroleum gases		237	218
GA1		211	191
GA2		210	190
GL1		209	188
GT1		209	188
Gsist		205	186

Table 11
CARBON EMISSION FACTOR
OF ANALYSED FUELS

It is seen that, for lignite, the carbon dioxide emission relative to the net calorific value is the highest, $\epsilon_{CO_2, I, Lignite} = 1396 \text{ g CO}_2/\text{kWh}$, whereas shale gas has the lowest value, $\epsilon_{CO_2, S, Gsist} = 205 \text{ g CO}_2/\text{kWh}$.

As regards the carbon dioxide emission relative to the gross calorific value, table 11 shows that lignite has the highest value, $\epsilon_{CO_2, S, Lignite} = 1136 \text{ g CO}_2/\text{kWh}$, whereas shale gas has the lowest value, $\epsilon_{CO_2, S, Gsist} = 186 \text{ g CO}_2/\text{kWh}$.

The highest values of the carbon dioxide emission factor are obtained for solid fuels, namely:

$$\epsilon_{CO_2, S, Lignite} > \epsilon_{CO_2, S, Hardwood} > \epsilon_{CO_2, S, Softwood} > \\ > \epsilon_{CO_2, S, Coal} > \epsilon_{CO_2, S, Anthracite}$$

As for biofuels, table 11 shows that:

$$\epsilon_{CO_2, I, Methyl\ linoleate} > \epsilon_{CO_2, I, Ethyl\ stearate} > \epsilon_{CO_2, I, Ethanol}$$

As shown in table 11, petrol and ethanol blending leads to the reduction of carbon dioxide emissions.

The new European Directives require that starting 1 January 2018 Romania should introduce on the market petrol with a biofuel content of at least 8% by volume. As of 1 January 2016, diesel fuel must have a biofuel content of at least 6.5% by volume. Biofuels are fuels produced from renewable resources, and their use reduces carbon dioxide emissions [14].

According to the National Institute of Statistics, in 2016 biofuel consumption in transport increased by 4.46% compared to the year 2000.

According to the data provided by S.C. Enel Energie Muntenia S.A., the CO₂ emission factor in Romania for the year 2016 was 287.11 g/kWh.

Conclusions

From a qualitative point of view, the evaluation of the carbon dioxide emission factor provides a hierarchy of the main fuels used.

From a quantitative point of view, the amount of carbon dioxide that reaches the atmosphere can be estimated for each fuel type.

Depending on the amount of carbon dioxide released by combustion, a strategy for each fuel category/type can be created.

The carbon dioxide emission factor can be used as an additional criterion for making decisions regarding fuel choice and energy strategy.

Nomenclature

g_i - Mass fraction of component i in a gas mixture, kg component i /kg fuel;

H - Caloric Power, kJ/kg, kJ/m³_N;

M - Molar Mass, kg/kmol;

m - Mass, kg;

r_i - Volumetric fraction of component i in a gas mixture, m³_N component i /m³_N fuel;

V - Volume, m³;

ϵ_{CO_2} - Carbon dioxide emission, g/kWh;

ρ_{15} - Relative density (the density of the liquid petroleum fuels relative to the water, at 15°)

Subscript

C - Carbon

CO₂ - carbon dioxide

H - Hydrogen

I - Inferior

m - coefficient

n - coefficient

O - Oxygen

r - coefficient

S - Superior

References

- ***http://www.minind.ro/dezbateri_publice/2011/strategia_energetica_20112035_20042011.pdf
- *** Anexa 1 la Hotararea Guvernului nr. 739/2016 -Strategia naionala privind schimbarile climatice si cresterea economica bazata pe emisii reduce
- *** <https://www.green-report.ro/emisii-de-co2-au-scazut-romania>

4. AVRAM, L., CRISTESCU, T., STOICA, M.E., Carbon Dioxide Emissions Monitoring in Romania in the Context of Greenhouse Gases Reduction, The first International Conference on Energy, Power, Petroleum and Petrochemical Engineering, Lebanese University, Beirut, Lebanon, April 26-28, 2017, p.104-106, IEEE.
5. CRISTESCU, T., STOICA, M.,E., Evaluation of the Emission of Carbon Dioxide in the Combustion of Biofuels and Comparison with Liquid Petroleum Products, Indian Journal of Applied Research, vol 3, Issue 10, October, 2013, pg. 28-30.
6. CRISTESCU, T., STOICA, M.-E., BRANOIU, GH., NEGREANU-PIRJOL, T., Evaluation and Comparing of the Carbon Dioxide Emission Coefficients for the Combustion of Gaseous and Liquid Hydrocarbons, Rev. Chim (Bucharest), **65**, no.7, 2014, p.856-860.
7. RAZNJEVIC, K., Tabele si diagrame termodinamice, Editura Tehnica, Bucuresti, 1978, p. 327.
8. ***www.insse.ro
9. AVRAM, L., CRISTESCU, T., STOICA, M, Energy Management Strategies in the Oil Industry for Chemical and Thermal Environment Pollution Reduction, MATEC Web Conf. Volume 121, 2017, 8th International Conference on Manufacturing Science and Education - MSE2017 Trends in New Industrial Revolution, <https://doi.org/10.1051/mateconf/201712109001>.
10. CRISTESCU,T., Termotehnica, Ed. University of Ploiesti, Ploie^oti, 2009, p. 145.
11. CERNEA, A.,R., DOBRINESCU, D., FAGARASANU, I., COVACI, A., Termotehnica, Editura Diactica si Pedagogica, Bucuresti, 1969, p. 273.
12. DAOLUN LI, LONGJUN ZHANG, JOHN YILIN WANG, DETANG LU, Composition - Transient Analysis in Shale - Gas Reservoirs With Consideration of Multicomponent Adsorption, SPE Journal, Aprilie 2016, p. 648-664
13. MARINESCU, M., STEFANESCU D., CHISACOF, AL., ADLER, O., Instalatii de ardere - culegere de probleme pentru ingineri, Editura Tehnica, Bucuresti, 1985
- 14.*** <http://www.economica.net>

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